

ENGINEERING SELECTION

STEP 1: Calculate the heat load

The heat load in BTU/HR or (Q) can be derived by using several methods. To simplify things, we will consider general specifications for hydraulic system oils and other fluids that are commonly used with shell & tube heat exchangers.

Terms			
GPM	= Gallons Per Minute	Kw	= Kilowatt (watts x 1000)
CN	= Constant Number for a given fluid	T _{in}	= Hot fluid entering temperature in °F
ΔT	= Temperature differential across the potential	T _{out}	= Hot fluid exiting temperature in °F
PSI	= Pounds per Square Inch (pressure) of the operating side of the system	t _{in}	= Cold fluid temperature entering in °F
MHP	= Horsepower of the electric motor driving the hydraulic pump	t _{out}	= Cold fluid temperature exiting in °F
		Q	= BTU / HR

For example purposes, a hydraulic system has a **125 HP (93Kw)** electric motor installed coupled to a pump that produces a flow of **80 GPM @ 2500 PSIG**. The temperature differential of the oil entering the pump vs exiting the system is about **5.3°F**. Even though our return line pressure operates below 100 psi, we must calculate the system heat load potential (Q) based upon the prime movers (pump) capability. We can use one of the following equations to accomplish this:

To derive the required heat load (Q) to be removed by the heat exchanger, apply ONE of the following. Note: The calculated heat loads may differ slightly from one formula to the next. This is due to assumptions made when estimating heat removal requirements. The factor (v) represents the percentage of the overall input energy to be rejected by the heat exchanger. The (v) factor is generally about 30% for most hydraulic systems, however it can range from 20%-70% depending upon the installed system components and heat being generated (ie. servo valves, proportional valves, etc...will increase the percentage required).

FORMULA	EXAMPLE
A) Q = GPM x CN x actual ΔT	A) Q = 80 x 210 x 5.3°F = 89,040 BTU/HR
B) Q = [(PSI x GPM) / 1714] x (v) x 2545	B) Q = [(2500x80)/1714] x .30 x 2545 = 89,090 BTU/HR
C) Q = MHP x (v) x 2545	C) Q = 125 x .30 x 2545 = 95,347 BTU/HR
D) Q = Kw to be removed x 3415	D) Q = 28 x 3415 = 95,620 BTU/HR
E) Q = HP to be removed x 2545	E) Q = 37.5 x 2545 = 95,437 BTU/HR

Constant for a given fluid (CN)	
1) Oil	CN = 210
2) Water	CN = 500
3) 50% E. Glycol	CN = 450

STEP 2: Calculate the Mean Temperature Difference

When calculating the MTD you will be required to choose a liquid flow rate to derive the cold side ΔT. If your water flow is unknown you may need to assume a number based on what is available. As a normal rule of thumb, for oil to water cooling a 2:1 oil to water ratio is used. For applications of water to water or 50 % Ethylene Glycol to water, a 1:1 ratio is common.

FORMULA	EXAMPLE
HOT FLUID ΔT = $\frac{Q}{CN \times GPM}$ Oil	ΔT = $\frac{89,090 \text{ BTU/hr (from step 1, item B)}}{210 \text{ CN} \times 80 \text{ GPM}} = 5.3^\circ\text{F} = \Delta T \text{ Rejected}$
COLD FLUID Δt = $\frac{BTU / hr}{CN \times GPM}$ Water	Δt = $\frac{89,090 \text{ BTU/hr}}{500 \text{ CN} \times 40 \text{ GPM (for a 2:1 ratio)}} = 4.45^\circ\text{F} = \Delta T \text{ Absorbed}$
T _{in} = Hot Fluid entering temperature in degrees F	T _{in} = 125.3 °F
T _{out} = Hot Fluid exiting temperature in degrees F	T _{out} = 120.0 °F
t _{in} = Cold Fluid entering temperature in degrees F	t _{in} = 70.0 °F
t _{out} = Cold Fluid exiting temperature in degrees F	t _{out} = 74.5 °F
$\frac{T_{out} - t_{in}}{T_{in} - t_{out}} = \frac{S[\text{smaller temperature difference}]}{L[\text{larger temperature difference}]} = \left(\frac{S}{L}\right)$	$\frac{120.0^\circ\text{F} - 70.0^\circ\text{F} = 50.0^\circ\text{F}}{125.3^\circ\text{F} - 74.5^\circ\text{F} = 50.8^\circ\text{F}} = \frac{50.0^\circ\text{F}}{50.8^\circ\text{F}} = .984$

STEP 3: Calculate Log Mean Temperature Difference (LMTD)

To calculate the LMTD please use the following method;

L = Larger temperature difference from step 2.

M = Natural log for the S/L number (LOCATED IN TABLE A). Note: If your calculator has the "natural log" function you may use it.

$$LMTD_i = L \times M$$

$$LMTD_i = 50.8 \times .992 \text{ (FROM TABLE A)} = 50.39$$

To correct the LMTD_i for a multipass heat exchangers calculate R & K as follows:

FORMULA	EXAMPLE
$R = \frac{T_{in} - T_{out}}{t_{out} - t_{in}}$	$R = \frac{125.3^\circ\text{F} - 120^\circ\text{F}}{74.5^\circ\text{F} - 70^\circ\text{F}} = \frac{5.3^\circ\text{F}}{4.5^\circ\text{F}} = \{1.17=R\}$
$K = \frac{t_{out} - t_{in}}{T_{in} - t_{in}}$	$K = \frac{74.5^\circ\text{F} - 70^\circ\text{F}}{124.5^\circ\text{F} - 70^\circ\text{F}} = \frac{4.5^\circ\text{F}}{55.4^\circ\text{F}} = \{0.081=K\}$

Locate the correction factor CF _B (FROM TABLE B) LMTD _c = LMTD _i x CF _B LMTD _c = 50.39 x 1 = 50.39

STEP 4: Calculate the area required

$$\text{Required Area sq.ft.} = \frac{Q \text{ (BTU / HR)}}{\text{LMTD}_c \times U \text{ (FROM TABLE C)}} = \frac{89,090}{50.39 \times 100} = 17.68 \text{ sq.ft.}$$

STEP 5: Selection

a) From TABLE E choose the correct series size, baffle spacing, and number of passes that best fits your flow rates for both shell and tube side. Note that the tables suggest minimum and maximum information. Try to stay within the 20-80 percent range of the indicated numbers.

Example

Oil Flow Rate = 80 GPM = Series Required from Table E = **1200 Series**
 Baffle Spacing from Table E = **C baffle**
 Water Flow Rate = 40 GPM = Passes required in 1200 series = **4 (FP)**

b) From TABLE D choose the heat exchanger model size based upon the sq.ft. or surface area in the series size that will accommodate your flow rate.

Example

Required Area = 17.68sq.ft Closest model required based upon sq.ft. & series = **AB-1202-C4-FP**

If you require a computer generated data sheet for the application, or if the information that you are trying to apply does not match the corresponding information, please contact our engineering services department for further assistance.

TABLE A- FACTOR M/LMTD = L x M

S/L	M	S/L	M	S/L	M	S/L	M
.01	.215	.25	.541	.50	.721	.75	.870
.02	.251	.26	.549	.51	.728	.76	.864
.03	.277	.27	.558	.52	.734	.77	.879
.04	.298	.28	.566	.53	.740	.78	.886
		.29	.574	.54	.746	.79	.890
.05	.317	.30	.582	.55	.753	.80	.896
.06	.334	.31	.589	.56	.759	.81	.902
.07	.350	.32	.597	.57	.765	.82	.907
.08	.364	.33	.604	.58	.771	.83	.913
.09	.378	.34	.612	.59	.777	.84	.918
.10	.391	.35	.619	.60	.783	.85	.923
.11	.403	.36	.626	.61	.789	.86	.928
.12	.415	.37	.634	.62	.795	.87	.934
.13	.427	.38	.641	.63	.801	.88	.939
.14	.438	.39	.648	.64	.806	.89	.944
.15	.448	.40	.655	.65	.813	.90	.949
.16	.458	.41	.662	.66	.818	.91	.955
.17	.469	.42	.669	.67	.823	.92	.959
.18	.478	.43	.675	.68	.829	.93	.964
.19	.488	.44	.682	.69	.836	.94	.970
.20	.497	.45	.689	.70	.840	.95	.975
.21	.506	.46	.695	.71	.848	.96	.979
.22	.515	.47	.702	.72	.852	.97	.986
.23	.524	.48	.709	.73	.858	.98	.991
.24	.533	.49	.715	.74	.864	.99	.995

TABLE D- Surface Area

Model Number	Surface Area in Sq.ft.			Model Number	Surface Area in Sq.ft.		
	1 / 4" O.D Tubing	3 / 8" O.D Tubing	5 / 8 O.D Tubing		1 / 4" O.D Tubing	3 / 8" O.D Tubing	5 / 8 O.D Tubing
AB-401	1.4	-	-	AB-1602	44.4	30.3	17.6
AB-402	3.0	-	-	AB-1603	66.3	45.3	26.5
AB-403	4.6	-	-	AB-1604	88.3	60.3	35.3
				AB-1605	110.3	75.6	44.1
AB-701	3.6	2.6	-	AB-1606	132.3	90.4	53.0
AB-702	7.3	5.2	-	AB-1607	154.3	105.4	61.8
AB-703	11.1	7.9	-	AB-1608	176.3	120.4	70.6
AB-704	14.9	10.6	-	AB-1609	197.9	135.2	79.5
AB-705	18.7	13.3	-	AB-1610	219.9	150.2	88.3
				AB-1611	241.9	165.2	97.1
AB-1002	17.7	11.2	5.9	AB-1612	263.9	180.2	105.9
AB-1003	26.5	16.8	8.8	AB-1613	285.9	195.2	114.7
AB-1004	35.4	22.4	11.8				
AB-1005	44.3	28.0	14.7	AB-2004	155.1	110.7	60.8
AB-1006	53.2	33.6	17.6	AB-2005	193.8	138.4	76.1
				AB-2006	232.6	166.1	91.3
AB-1202	25.5	17.9	8.8	AB-2007	271.4	193.8	106.5
AB-1203	38.0	26.7	13.2	AB-2008	310.2	221.4	121.7
AB-1204	50.3	35.4	17.6	AB-2009	349.0	249.1	137.0
AB-1205	63.0	44.2	22.1	AB-2010	387.7	276.8	152.2
AB-1206	75.6	53.2	26.5	AB-2011	426.5	304.5	167.4
AB-1207	88.2	62.0	30.9	AB-2012	465.3	332.2	182.7
AB-1208	100.6	70.7	35.3	AB-2013	504.1	359.9	197.9
AB-1209	113.0	79.4	39.6	AB-2014	542.9	387.6	213.2
AB-1210	125.4	88.1	44.1	AB-2015	581.7	415.3	228.4

TABLE B- LMTD correction factor for Multipass Exchangers

R	P														
	.05	.1	.15	.2	.25	.3	.35	.4	.45	.5	.6	.7	.8	.9	1.0
.2	1	1	1	1	1	1	1	.999	.993	.984	.972	.942	.908	.845	.71
.4	1	1	1	1	1	1	.994	.983	.971	.959	.922	.855	.70		
.6	1	1	1	1	1	.992	.980	.965	.948	.923	.840				
.8	1	1	1	1	.995	.981	.965	.945	.916	.872					
1.0	1	1	1	1	.988	.970	.949	.918	.867	.770					
2.0	1	1	.997	.973	.940	.845	.740								
3.0	1	1	.997	.933	.835										
4.0	1	.993	.950	.850											
5.0	1	.982	.917												
6.0	1	.968	.855												
8.0	1	.930													
10.0	.996	.880													
12.0	.985	.720													
14.0	.972														
16.0	.958														
18.0	.940														
20.0	.915														

TABLE E- Flow Rate for Shell & Tube

Shell dia .	Max. Liquid Flow - Shell Side					Liquid Flow - Tube Side					
	Baffle Spacing					SP		TP		FP	
	A	B	C	D	E	Min.	Max.	Min.	Max.	Min.	Max.
400	10	15	20	—	—	3.5	21	—	—	—	—
700	17	29	30	35	—	9	61	4.5	30	2.2	15
800	20	35	40	—	—	10	50	4.5	38	3	21
1000	24	48	68	70	—	20	120	10	70	5.0	37
1200	29	56	105	115	120	30	250	15	112	7.5	56
1600	38	70	150	200	220	57	460	29	180	14	90
2000	—	—	190	370	550	90	650	45	320	25	160

TABLE C

U	TUBE FLUID	SHELL FLUID
400	Water	Water
350	Water	50% E. Glycol
100	Water	Oil
300	50% E. Glycol	50% E. Glycol
90	50% E. Glycol	Oil