



website: www.aihti.com

general email: sales@aihti.com technical email: engineering@aihti.com

## Shell & Tube Application Request: (For steam to liquid heat exchangers)

For UCN, URCN, & UCF, URCF Series

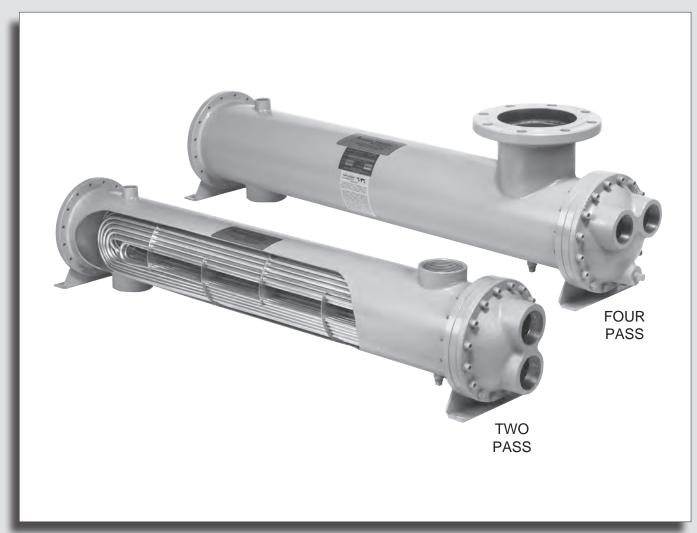
E	Email form to: sales@aihti.com or er	ngineering@aihti.com or fax to 434-757-1810
Contact Name _		Telephone Date
Company Name		Email
Address:		Fax
	Heated Fluid	Hot Side
	Fluid Type	Fluid Steam
	Density lb/ft3	1. Steam Pressure
If available	Viscosity cP	2. Temperature In
ii availabit	Conductivity Btu/hr.ft.°F  Specific Heat Btu/lb.°F	3. Flow Rate of steam
	Specific Heat Blumb. 1	
	1. Flow Rate	4. Heat Load
	2. Temperature In	
	3. Temperature Out:	
	4. Maximum Allowable Pressure Drop:	
То	properly size the heat exchanger we need 3 of	the 4 perameter on the Hot Side and 2 on the Cold Side.
Shell Material C	onstruction:	Tube Material Construction:
Brass Stee	el ☐ Stainless Steel ☐	Copper ☐ 90/10 Copper Nickel ☐ Stainless Steel ☐
ASME Code an		Require All Stainless Steel Heat Exchanger Yes \( \text{ No } \)
Comment:		



Manufacturer of Quality Heat Exchangers



#### UCN, URCN & UCF, URCF SERIES



#### **U-TUBE FIXED & REMOVEABLE BUNDLE**

# **HEAT EXCHANGERS**

## For steam to liquid service

- Operating pressure for tubes 100 PSI.
- Operating pressure for shell 100 PSI.
- Operating temperature 400 °F.
- Can be customized to fit any application.
- Computer generated data sheet available for any application
- · As an option, available in ASME Code and Certified

# UCN, URCN, UCF & URCF Series overview



#### UCN, URCN SERIES

U-tube heat exchangers with fixed or removeable tube bundle for steam service. Normally applied when the differential temperature between the hot fluid entering and the cooling fluid entering is 150°F or greater. U-tube design allows tubing to freely expand and contract independently of the shell. Welded outer shell construction made of carbon steel with NPT connection ports. Sizes from 5" to 10" diameters. Standard two and four pass units available. Optional 90/10 copper nickel, stainless steel, and carbon steel tube. Can be modified to meet your requirements.



#### **UCF & URCF SERIES**

U-tube heat exchangers with fixed or removeable tube bundle for steam service. Normally applied when the differential temperature between the hot fluid entering and the cooling fluid entering is 150°F or greater. U-tube design allows tubing to freely expand and contract independently of the shell. Welded outer shell construction made of carbon steel with ANSI flange ports. Sizes from 5" to 10" diameters. Standard two and four pass units available. Optional 90/10 copper nickel, stainless steel, and carbon steel tube. Can be modified to meet your requirements.



#### STANDARD URCS STOCK UNIT FOR STEAM APPLICATION

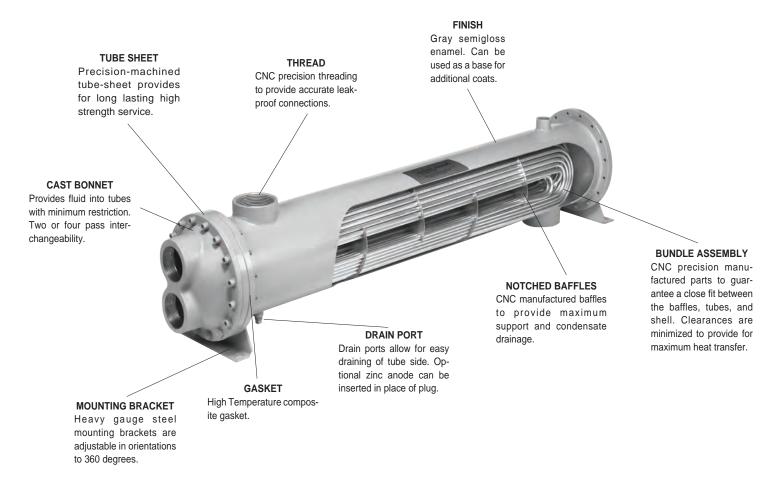
U-tube heat exchangers with removeable tube bundle for fluids with high differential inlet temperatures or where tube bundle requires removal. Normally applied when the differential temperature between the hot fluid entering and the cooling fluid entering is 150°F or greater. U-tube design allows tubing to freely expand and contract independently of the shell. Welded outer shell construction made of carbon steel with NPT or ANSI flange ports and viton o-ring seals. Sizes from 4" to 8" diameters. Standard Two Pass units available. Can be modified to meet your requirements. See page 140 for detailed dimension.



#### **ACW / AOCHW SERIES**

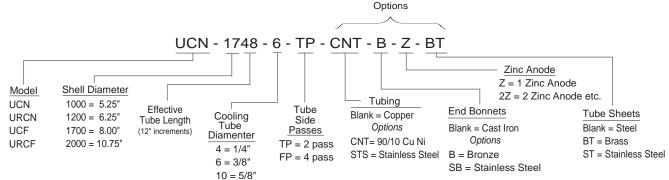
Can be used as a Space heater by using steam or hot water

# UCN, URCN, UCF & URCF Series construction



#### **UNIT CODING**





#### STANDARD CONSTRUCTION MATERIALS & RATINGS

Standard Model	UCN / URCN & UCF / URCF	Options	Standard Unit Ratings		
Shell	Steel	Steel Stainless Steel			
Tubes	Copper	90/10 Cu. Ni. / Stainless Steel	Operating Pressure Tubes		
Baffles	Aluminum / Brass	Stainless Steel	100 psig		
Tube Sheet	Steel	Brass / Stainless Steel	Operating Pressure Shell		
End Bonnets	Cast Iron	Stainless Steel	100 psig		
Mounting Brackets	Steel	Stainless Steel	Operating Temperature  400 °F		
Gasket	High Temperature Gasket	Viton	400 -F		

#### Example [A] Calculate surface area required.

Heat 50gpm fresh water from  $70^{\circ}F$  to  $170^{\circ}F$ , using saturated steam at 50psig.

 $T_s$  = Steam temperature  $^{\rm O}F$  $t_{\rm in}$  = Cold Side entering fluid  $^{\rm O}F$  $t_{\rm out}$  = Cold Side exiting fluid  $^{\rm O}F$ 

Step 1. Calculate the heat load Btu/hr [Q].

 $Q = GPM \ x \ CN \ x \ \triangle T$  $Q = 50gpm \ x \ 500 \ x \ (170^{o}F-70^{o}F) = 2,500,000 \ Btu/hr$ 

Step 2 Acquire steam temperature and enthalpy from graphs T&L

 $50psig = 297^oF$  steam. From graph **T** (pg. 110). 50psig = 912 Btu/lb. From graph **L** (pg. 111).

Step 3. Calculate the mean temperature difference (MTD)

$$\frac{T_{s} - t_{in}}{T_{s} - t_{out}} = \frac{297^{\circ}F - 70^{\circ}F}{297^{\circ}F - 170^{\circ}F} = \frac{227^{\circ}F \text{ (Larger) L}}{127^{\circ}F \text{ (Smaller) S}}$$

$$\frac{S}{L} = \frac{127^{\circ}F}{227^{\circ}F} = .559$$
 Go to Table A .559 = .758

Find the LMTD = [.758 x (L) 227] = 172.0

Step 4. Calculate the surface area required.

$$A_s \ = \ \frac{Q \ (Btu/hr)}{LMTD \ x \ U} \ = \ \frac{2,500,000}{172 \ x \ 300} = \ 48.4 \ sq. \ ft.$$

Step 5. Calculate the Capacity Factor [F] for steam.

$$F_c = \frac{Q}{Btu/lb} = \frac{2,500,000 \text{ Btu/hr}}{912 \text{ Btu/lb}} = 2,741.3 \text{ lbs/hr steam}$$

Step 6. Select a the proper diameter heat exchanger using graphs F or G and  $F_c$  from step 5.

Capacity = 2741.3 @ 50psig = 1700 series 3/8 or 5/8 tubes from chart (G).

Use table  $\bf D$  to determine the final heat exchanger size. 48.4 sq.ft. =  $\bf URCF-1748-6-TP$ 

#### Application [B] Calculate using the graphs.

Heat 70gpm fresh water from 50°F to 180°F using 65psig saturated steam.

Step 1. Calculate the heat load Btu/hr [Q].

Q = GPM x CN x  $\triangle$ T Q = 70 x 500 x (180°F - 50°F) = 4,550,000 Btu/hr

Step 2. Derive the steam temperature  $[T_s]$  from the graph  $\mathbf{T}$ . Derive the capacity factor  $[F_s]$  from graph  $\mathbf{L}$ .

65psig = 312°F steam. From graph **T** 65psig = 901 Btu/lb. From graph **L** 

Step 3. Calculate the  $F_{\circ}$  required.

$$F_s = \frac{Btu/hr[Q]}{T_s - t_{out}} = \frac{4,550,000}{312^oF - 180^oF} = 34,470$$

Step 4. Calculate the Capacity Factor  $F_c$  for steam.

$$F_c = \frac{Q}{Btu/lb} = lbs/hr$$
  $\frac{2,500,000 Btu/hr}{912 Btu/lb} = 5,050 lbs/hr steam}{required}$ 

Step 5. Select the proper diameter heat exchanger using the capacity graphs F or G and F from step 4.

Capacity = 5050 = 2000 series with 5/8" Tubes.

Step 6. Select the proper size heat exchanger from the performance curves corresponding to the series selected using the capacity factor. Select the heat exchanger closest to the line landing on or above the calculated point.

 $F_s = 34,470 \text{ Btu/hr } f = \text{URCF } 2084-6-\text{TP}$ 

#### Application [C] Calculate batch heating of a tank.

Heat a 1000 gallon stainless steel tank of water from  $50^{\circ}F$  to  $150^{\circ}F$  in 1.5 hours using 40psig saturated steam, circulating at 30gpm. Tank size 6ft w x 6ft h x 6ft d. Ambient air temperature  $60^{\circ}F$  worse case.

Step 1. Calculate the total heat load [Q] Btu/hr.

Q = Total Gallons x lbs/gallon x Specific heat Btu/lb x  $\triangle$ T Q = 1000 x 8.34 x 1.0 x 100°F = 834,000 Btu

Corrected Q for time = 
$$\frac{834,000 \times 60 \text{ min}}{(1.5 \text{hours}) \times 60 \text{ min}} = 556,00 \text{ Btu/hr}$$

Step 2. Calculate the  $\triangle T_{average}$   $(T_a)$  for the heated water.

$$\triangle T_a = \frac{T_f - T_i}{2} + T_i$$
  $T_a = \frac{150^{\circ}F - 50^{\circ}F}{1.5 \text{ hours}} + 50^{\circ}F = 116.7^{\circ}F$ 

 $\begin{array}{l} Q_{Loss} = Surface \ area \ tank \ sq.ft \ x \ .001 \ x \ \triangle t_a \ x \ 2545 \\ Q_{Loss} = 6x6x6 \ x \ .001 \ x \ (116.7^oF_a\text{--} \ 60^oF) \ x \ 2545 = 31,169 \ Btu/hr \end{array}$ 

$$Q_t = Q + Q_{Loss} = Q_t$$
 556,000 + 31,169 = 587,169 Btu/hr

Step 3. Derive the steam temperature  $[T_s]$  from graph T. Derive the capacity factor from graph L.

Given 40psig saturated steam = 287<sup>o</sup>F steam acquired from graph T.

Given 40psig saturated steam = 920 Btu/lb acquired from graph L.

Step 4. Calculate the mean temperature difference (MTD)

$$\frac{T_{s} - T_{a}}{T_{s} - T_{e}} = \frac{287^{o}F - 100^{o}F}{287^{o}F - 150^{o}F} = \frac{187^{o}F}{137^{o}F}$$

$$\frac{S}{L} = \frac{137^{\circ}F}{187^{\circ}F} = .732 \text{ Goto Table A. } .732 = .659$$

Calculate the Log mean temperature difference LMTD

 $LMTD = [.659 \text{ x (L) } 187^{\circ}\text{F}] = 123.2$ 

Step 5. Calculate the required surface area

$$A_s = \ \frac{Q}{LMTD \ x \ U} \quad = \ \frac{587,169 \ Btu/hr}{123.2 \ x \ 300} \quad = \ 15.9 \ sq. \ ft.$$

note: AIHTI reserves the right to make reasonable design changes without notice.

Step 6. Select the proper diameter heat exchanger by calculating the capacity factor.

$$F_c = \frac{Q}{Btu/lb} = lbs/hr$$
  $\frac{587,169 Btu/hr}{920 Btu/lb} = 639 lbs/hr$ 

From graph F or G select the proper diameter heat exchanger. Capacity 639 lbs/hr saturated steam required @ 40psig.

Capacity = 639 lbs/hr = 1000 series 3/8" tubes

Step 7. Select the proper size heat exchanger from the surface area chart in table D.

Minimum surface area required = 15.9 sq.ft. = URCN1036-6-TP

TABLE A- FACTOR M/LMTD = L x M

S/L	M	S/L	М	S/L	M	S/L	M
.01 .02 .03 .04	.215 .251 .277 .298	.25 .26 .27 .28 .29	.541 .549 .558 .566 .574	.50 .51 .52 .53 .54	.721 .728 .734 .740 .746	.75 .76 .77 .78 .79	.870 .874 .879 .886 .890
.05 .06 .07 .08 .09	.317 .334 .350 .364 .378	.30 .31 .32 .33	.582 .589 .597 .604 .612	.55 .56 .57 .58 .59	.753 .759 .765 .771 .777	.80 .81 .82 .83 .84	.896 .902 .907 .913
.10 .11 .12 .13 .14	.391 .403 .415 .427 .438	.35 .36 .37 .38 .39	.619 .626 .634 .641 .648	.60 .61 .62 .63 .64	.783 .789 .795 .801 .806	.85 .86 .87 .88	.923 .928 .934 .939 .944
.15 .16 .17 .18 .19	.448 .458 .469 .478 .488	.40 .41 .42 .43 .44	.655 .662 .669 .675	.65 .66 .67 .68 .69	.813 .818 .823 .829 .836	.90 .91 .92 .93 .94	.949 .955 .959 .964 .970
.20 .21 .22 .23 .24	.497 .506 .515 .524 .533	.45 .46 .47 .48 .49	.689 .695 .702 .709 .715	.70 .71 .72 .73 .74	.840 .848 .852 .858 .864	.95 .96 .97 .98	.975 .979 .986 .991 .995

Step 8. Select same using the performance chart.

$$F_s = \frac{Btu/hr}{T_s - T_{ovit}} = \frac{587,169}{287 - 150} = 4,286 F_s$$

From the chart 1000, 3/8" tubes on page () select unit landing closest on or above intersection point of 30gpm & 4,286 Btu/hr <sup>o</sup>F

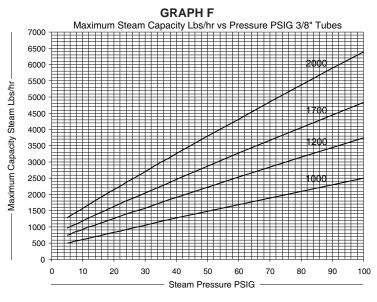
Selection = URCN1036-6-TP

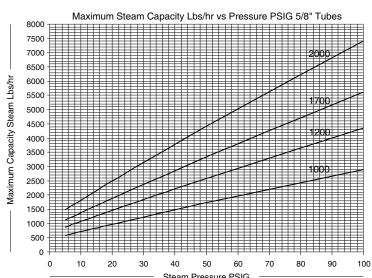
TABLE D- Surface Area

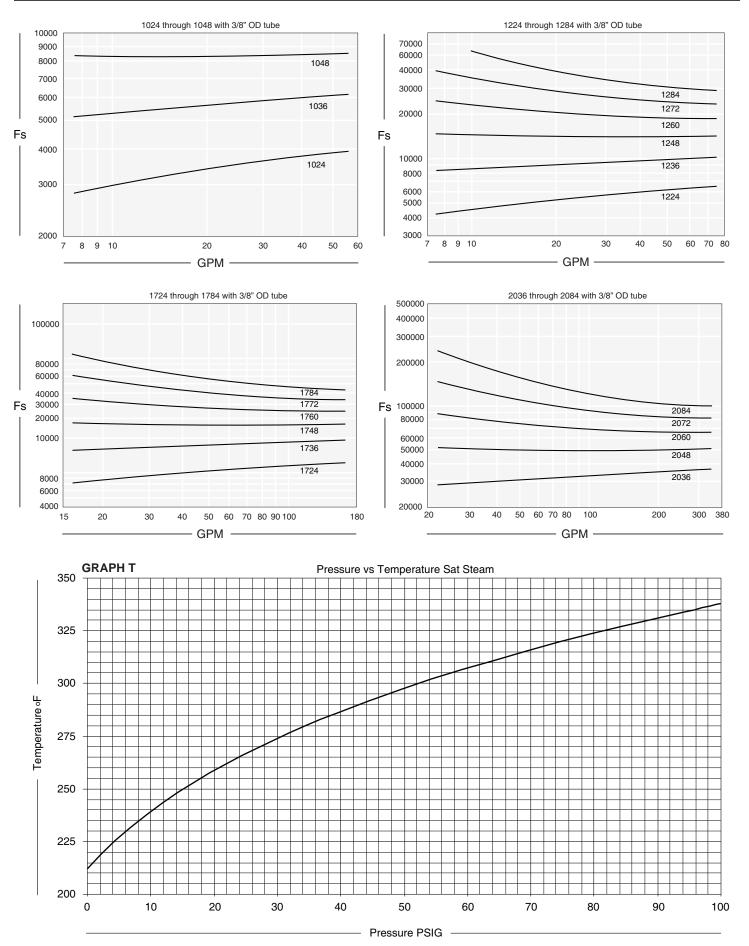
	Surface Are	ea in Sq.ft.		Surface Ar	ea in Sq.ft.
Model	3/8" O.D	5/8" O.D	Model	3/8" O.D	5/8" O.D
Number	Tubing	Tubing	Number	Tubing	Tubing
	CODE 6	CODE 10		CODE 6	CODE 10
1024	11.0	6.5	1724	32.2	17.0
1036	16.5	9.8	1736	48.3	25.5
1048	22.0	13.0	1748	64.4	34.0
			1760	80.5	42.5
1224	17.3	9.1	1772	96.6	51.0
1236	25.9	13.7	1784	112.7	59.5
1248	34.5	18.3			
1260	43.2	22.9	2036	80.1	41.2
1272	51.8	27.5	2048	106.8	55.0
1284	60.5	32.0	2060	133.5	68.7
			2072	160.2	82.5
			2084	186.9	96.2

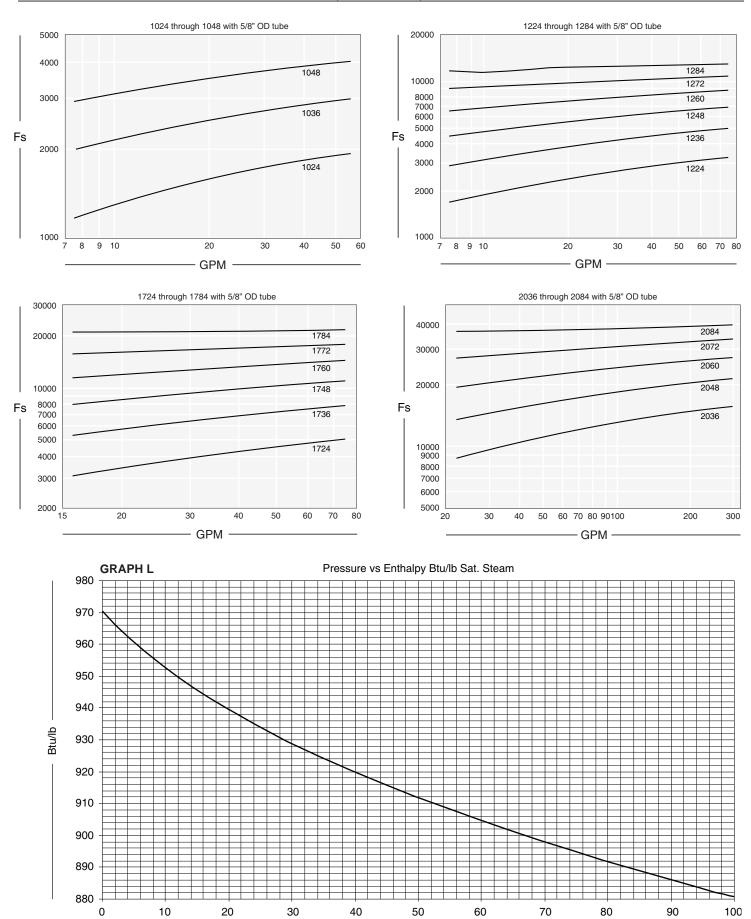
TABLE E- Flow Rate for Shell & Tube

	The state of the s								
Shell		Liquid Flow - Tube Side							
dia.	3/8'	'TP	5/8" TP		3/8'	'FP	5/8" FP		
Code	Min.	Max.	Min.	Max.	Min.	Max.	Min.	Max.	
1000	5	60	5	60	5	37	5	33	
1200	5	100	5	100	7.5	56	7.5	50	
1700	10	180	10	160	14	90	14	80	
2000	15	340	15	300	25	160	25	145	

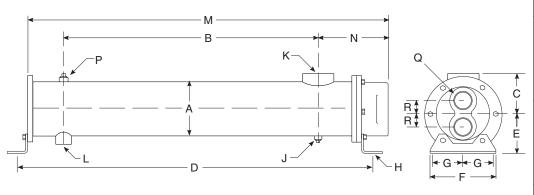






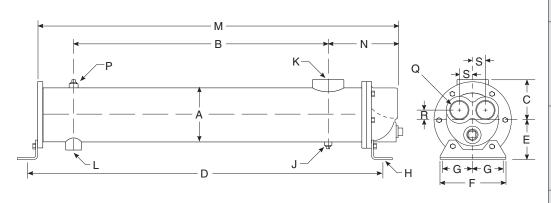


Pressure PSIG



Model	М	N	Q NPT	R
UCN-1024	28.88			
UCN-1036	40.88	6.00	1.50	1.19
UCN-1048	52.88			
UCN-1224	29.17			
UCN-1236	41.17			
UCN-1248	53.17	6.67	2 00	1.44
UCN-1260	65.17	0.07	2.00	1.44
UCN-1272	77.17			
UCN-1284	89.17			
UCN-1724	30.13			
UCN-1736	42.13			
UCN-1748	54.13	7.88	2.50	1.88
UCN-1760	66.13	7.00	2.50	1.00
UCN-1772	78.13			
UCN-1784	90.13			
UCN-2036	43.91			
UCN-2048	55.91			
UCN-2060	67.91	10.16	3.00	2.50
UCN-2072	79.91			
UCN-2084	91.91			

## Two Pass (TP)

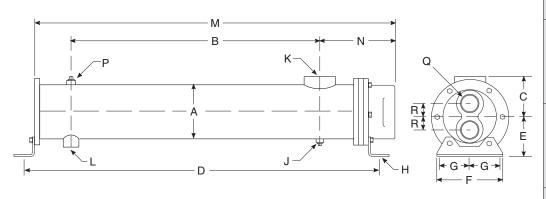


#### Model Μ Ν S UCN-1024 29.21 UCN-1036 41.21 6.34 1.00 .75 1.19 UCN-1048 53.21 UCN-1224 29.58 UCN-1236 41.58 UCN-1248 53.58 1.06 1.50 1.44 65.58 UCN-1260 UCN-1272 77.58 UCN-1284 84.58 UCN-1736 UCN-1748 53.78 2.00 1.38 1.88 UCN-1760 65.78 UCN-1772 77.78 UCN-1784 89.78 UCN-2036 UCN-2048 56.00 2.50 UCN-2060 68.00 10.26 2.50 1.75 UCN-2072 80.00 UCN-2084 92.00

# **FOUR PASS (FP)**

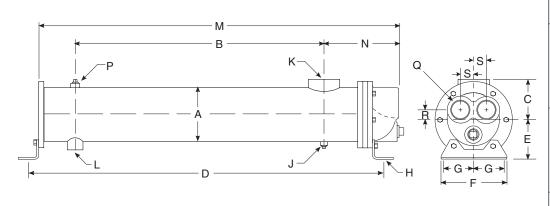
Model	А	В	С	D	Е	F	G	Н	J NPT	K NPT	L NPT	P NPT	Weight	Model
UCN-1024 UCN-1036 UCN-1048	5.25	20.00 32.00 44.00	3.69	29.13 41.13 53.13	4.00	5.25	2.00	.44 x 1.00 thru slot	.375	2.00	1.50	.75	55.00 70.00 85.00	UCN-1024 UCN-1036 UCN-1048
UCN-1224 UCN-1236 UCN-1248 UCN-1260 UCN-1272 UCN-1284	6.25	19.00 31.00 43.00 55.00 67.00 79.00	4.19	29.59 41.59 53.59 65.59 77.59 89.59	4.50	6.25	2.50	.44 x 1.00 thru slot	.375	2.50	2.00	.75	83.00 108.00 132.00 158.00 182.00 206.00	UCN-1224 UCN-1236 UCN-1248 UCN-1260 UCN-1272 UCN-1284
UCN-1724 UCN-1736 UCN-1748 UCN-1760 UCN-1772 UCN-1784	8.00	19.00 31.00 43.00 55.00 67.00 79.00	5.06	29.50 41.50 53.50 65.50 77.50 89.50	5.75	8.25	3.50	.44 x 1.00 thru slot	.375	3.00	2.00	1.00	138.00 180.00 219.00 258.00 300.00 342.00	UCN-1724 UCN-1736 UCN-1748 UCN-1760 UCN-1772 UCN-1784
UCN-2036 UCN-2048 UCN-2060 UCN-2072 UCN-2084	10.75	30.00 42.00 54.00 66.00 78.00	6.88	42.63 54.63 66.63 78.63 90.63	8.00	11.50	5.00	.781 x 1.25 thru slot	.50	4.00	3.00	1.25	620.00 670.00 730.00 820.00 870.00	UCN-2036 UCN-2048 UCN-2060 UCN-2072 UCN-2084

# **URCN** dimensions



Model	М	N	Q NPT	R	
URCN-1024	28.88				
URCN-1036	40.88	6.00	1.50	1.19	
URCN-1048	52.88				
URCN-1224	29.17				
URCN-1236	41.17				
URCN-1248	53.17	6.67	2 00	1 44	
URCN-1260	65.17	0.07	2.00	1.44	
URCN-1272	77.17				
URCN-1284	89.17				
URCN-1724	30.13				
URCN-1736	42.13				
URCN-1748	54.13	7.88	2.50	1.88	
URCN-1760	66.13	7.00	2.50	1.00	
URCN-1772	78.13				
URCN-1784	90.13				
URCN-2036	43.91				
URCN-2048	55.91				
URCN-2060	67.91	10.16	3.00	2.50	
URCN-2072	79.91				
URCN-2084	91.91				

## Two Pass (TP)

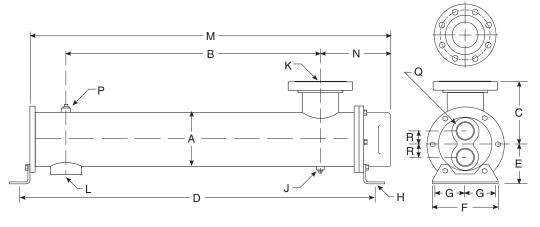


Model	М	N	Q NPT	R	S
URCN-1024 URCN-1036 URCN-1048	29.21 41.21 53.21	6.34	1.00	.75	1.19
URCN-1224 URCN-1236 URCN-1248 URCN-1260 URCN-1272 URCN-1284	29.58 41.58 53.58 65.58 77.58 84.58	7.08	1.50	1.06	1.44
URCN-1724 URCN-1736 URCN-1748 URCN-1760 URCN-1772 URCN-1784	29.78 41.78 53.78 65.78 77.78 89.78	7.53	2.00	1.38	1.88
URCN-2036 URCN-2048 URCN-2060 URCN-2072 URCN-2084	44.00 56.00 68.00 80.00 92.00	10.26	2.50	1.75	2.50

## **FOUR PASS (FP)**

Model	А	В	С	D	E	F	G	Н	J NPT	K NPT	L NPT	P NPT	Weight	Model
URCN-1024 URCN-1036 URCN-1048	5.25	20.00 32.00 44.00	3.69	29.13 41.13 53.13	4.00	5.25	2.00	.44 x 1.00 thru slot	.375	2.00	1.50	.75	55.00 70.00 85.00	URCN-1024 URCN-1036 URCN-1048
URCN-1224 URCN-1236 URCN-1248 URCN-1260 URCN-1272 URCN-1284	6.25	19.00 31.00 43.00 55.00 67.00 79.00	4.19	29.59 41.59 53.59 65.59 77.59 89.59	4.50	6.25	2.50	.44 x 1.00 thru slot	.375	2.50	2.00	.75	83.00 108.00 132.00 158.00 182.00 206.00	URCN-1224 URCN-1236 URCN-1248 URCN-1260 URCN-1272 URCN-1284
URCN-1724 URCN-1736 URCN-1748 URCN-1760 URCN-1772 URCN-1784	8.00	19.00 31.00 43.00 55.00 67.00 79.00	5.06	29.50 41.50 53.50 65.50 77.50 89.50	5.75	8.25	3.50	.44 x 1.00 thru slot	.375	3.00	2.00	1.00	138.00 180.00 219.00 258.00 300.00 342.00	URCN-1724 URCN-1736 URCN-1748 URCN-1760 URCN-1772 URCN-1784
URCN-2036 URCN-2048 URCN-2060 URCN-2072 URCN-2084	10.75	30.00 42.00 54.00 66.00 78.00	6.88	42.63 54.63 66.63 78.63 90.63	8.00	11.50	5.00	.781 x 1.25 thru slot	.50	4.00	3.00	1.25	620.00 670.00 730.00 820.00 870.00	URCN-2036 URCN-2048 URCN-2060 URCN-2072 URCN-2084

#### FIXED TUBE BUNDLE (U-TUBE DESIGN)



Model	М	N	Q NPT	R
UCF-1024	28.88			
UCF-1036	40.88	6.43	1.50	1.19
UCF-1048	52.88			
UCF-1224	29.17			
UCF-1236	41.17			
UCF-1248	53.17	7.23	2.00	1 44
UCF-1260	65.17	1.23	2.00	1.44
UCF-1272	77.17			
UCF-1284	89.17			
UCF-1724	30.13			
UCF-1736	42.13			
UCF-1748	54.13	8 64	2.50	4.00
UCF-1760	66.13	0.04	2.50	1.88
UCF-1772	78.13			
UCF-1784	90.13			
UCF-2036	43.91			
UCF-2048	55.91			
UCF-2060	67.91	11.07	3.00	2.50
UCF-2072	79.91			
UCF-2084	91.91			

## Two Pass (TP)

	м в	$\kappa$
		C
	<del>\</del>	J H G + G + G + F - F - F - F - F - F - F - F - F - F

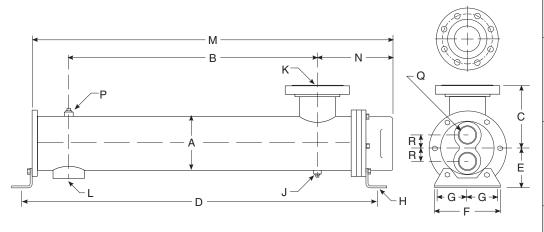
#### Μ Ν R S Model NPT UCF-1024 29.21 UCF-1036 41.21 6.77 1.00 .75 1.19 UCF-1048 53.21 UCF-1224 29.58 UCF-1236 41.58 UCF-1248 53.58 1.50 1.06 1.44 UCF-1260 65.58 UCF-1272 77.58 UCF-1284 84.58 UCF-1724 29.78 UCF-1736 41.78 UCF-1748 53.78 8.29 2.00 1.38 1.88 UCF-1760 65.78 UCF-1772 77.78 UCF-1784 89.78 UCF-2036 UCF-2048 56.00 UCF-2060 68.00 11.16 2.50 1.75 2.50 UCF-2072 80.00 UCF-2084 92.00

# **FOUR PASS (FP)**

Model	А	В	С	D	E	F	G	Н	J NPT	K ANSI Flange	L NPT	P NPT	Weight	Model
UCF-1024 UCF-1036 UCF-1048	5.25	19.75 31.75 43.75	7.63	29.13 41.13 53.13	4.00	5.25	2.00	.44 x 1.00 thru slot	.375	3.00	1.50	.75	55.00 70.00 85.00	UCF-1024 UCF-1036 UCF-1048
UCF-1224 UCF-1236 UCF-1248 UCF-1260 UCF-1272 UCF-1284	6.25	19.00 31.00 43.00 55.00 67.00 79.00	8.13	29.59 41.59 53.59 65.59 77.59 89.59	4.50	6.25	2.50	.44 x 1.00 thru slot	.375	4.00	2.00	.75	83.00 108.00 132.00 158.00 182.00 206.00	UCF-1224 UCF-1236 UCF-1248 UCF-1260 UCF-1272 UCF-1284
UCF-1724 UCF-1736 UCF-1748 UCF-1760 UCF-1772 UCF-1784	8.00	18.25 30.25 42.25 54.25 66.25 78.25	9.00	29.50 41.50 53.50 65.50 77.50 89.50	5.75	8.25	3.50	.44 x 1.00 thru slot	.375	5.00	2.00	1.00	138.00 180.00 219.00 258.00 300.00 342.00	UCF-1724 UCF-1736 UCF-1748 UCF-1760 UCF-1772 UCF-1784
UCF-2036 UCF-2048 UCF-2060 UCF-2072 UCF-2084	10.75	29.00 41.00 53.00 65.00 76.00	10.38	42.63 54.63 66.63 78.63 90.63	8.00	11.50	5.00	.781 x 1.25 thru slot	.50	6.00	3.00	1.25	620.00 670.00 730.00 820.00 870.00	UCF-2036 UCF-2048 UCF-2060 UCF-2072 UCF-2084

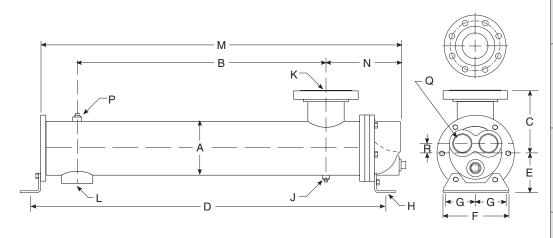
# **URCF Series** dimensions

## REMOVABLE TUBE BUNDLE (U-TUBE DESIGN)



Model	М	N	Q NPT	R
URCF-1024 URCF-1036	28.88 40.88	6.43	1.50	1.19
URCF-1048	52.88			
URCF-1224	29.17			
URCF-1236	41.17			
URCF-1248	53.17	7.23	2.00	1 44
URCF-1260	65.17	1.23	2.00	1.44
URCF-1272	77.17			
URCF-1284	89.17			
URCF-1724	30.13			
URCF-1736	42.13			
URCF-1748	54.13	8 64	2 50	1.88
URCF-1760	66.13	0.04	2.50	1.00
URCF-1772	78.13			
URCF-1784	90.13			
URCF-2036	43.91			
URCF-2048	55.91			
URCF-2060	67.91	11.07	3.00	2.50
URCF-2072	79.91			
URCF-2084	91.91			

## Two Pass (TP)

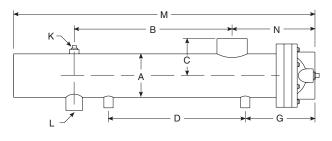


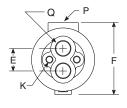
Model	М	N	Q NPT	R	S
URCF-1024 URCF-1036 URCF-1048	29.21 41.21 53.21	6.77	1.00	.75	1.19
URCF-1224 URCF-1236 URCF-1248 URCF-1260 URCF-1272 URCF-1284	29.58 41.58 53.58 65.58 77.58 84.58	7.64	1.50	1.06	1.44
URCF-1724 URCF-1736 URCF-1748 URCF-1760 URCF-1772 URCF-1784	29.78 41.78 53.78 65.78 77.78 89.78	8.29	2.00	1.38	1.88
URCF-2036 URCF-2048 URCF-2060 URCF-2072 URCF-2084	44.00 56.00 68.00 80.00 92.00	11.16	2.50	1.75	2.50

# **FOUR PASS (FP)**

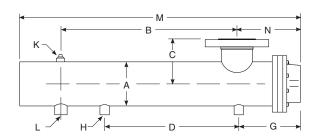
Model	А	В	С	D	E	F	G	Н	J NPT	K ANSI Flange	L NPT	P NPT	Weight	Model
URCF-1024 URCF-1036 URCF-1048	5.25	19.75 31.75 43.75	7.63	29.13 41.13 53.13	4.00	5.25	2.00	.44 x 1.00 thru slot	.375	3.00	1.50	.75	55.00 70.00 85.00	URCF-1024 URCF-1036 URCF-1048
URCF-1224 URCF-1236 URCF-1248 URCF-1260 URCF-1272 URCF-1284	6.25	19.00 31.00 43.00 55.00 67.00 79.00	8.13	29.59 41.59 53.59 65.59 77.59 89.59	4.50	6.25	2.50	.44 x 1.00 thru slot	.375	4.00	2.00	.75	83.00 108.00 132.00 158.00 182.00 206.00	URCF-1224 URCF-1236 URCF-1248 URCF-1260 URCF-1272 URCF-1284
URCF-1724 URCF-1736 URCF-1748 URCF-1760 URCF-1772 URCF-1784	8.00	18.25 30.25 42.25 54.25 66.25 78.25	9.00	29.50 41.50 53.50 65.50 77.50 89.50	5.75	8.25	3.50	.44 x 1.00 thru slot	.375	5.00	2.00	1.00	138.00 180.00 219.00 258.00 300.00 342.00	URCF-1724 URCF-1736 URCF-1748 URCF-1760 URCF-1772 URCF-1784
URCF-2036 URCF-2048 URCF-2060 URCF-2072 URCF-2084	10.75	29.00 41.00 53.00 65.00 76.00	10.38	42.63 54.63 66.63 78.63 90.63	8.00	11.50	5.00	.781 x 1.25 thru slot	.50	6.00	3.00	1.25	620.00 670.00 730.00 820.00 870.00	URCF-2036 URCF-2048 URCF-2060 URCF-2072 URCF-2084

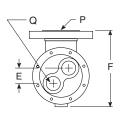
# Standard URCS stock unit for steam application



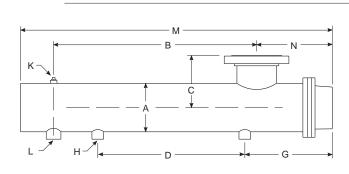


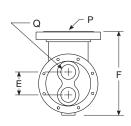
**URCS-830** 





URCS-1230, URCS-1242, URCS-1254





URCS-1754

#### **COMMON DIMENSIONS**

MODEL	А	В	С	D	Е	F	G	H NPT	K NPT	L NPT	M	N	Р	Q NPT	WEIGHT
URCS-830-25180	4.25	15.00	3.56	13.00	2.38	6.81	5.75	1.00	.38	1.25	28.63	7.88	2.5" NPT	1.25	35
URCS-1230-25182	6.25	13.00	6.38	13.00	3.12	10.75	5.75	1.00	_	1.50	27.75	9.00	4" ANSI	2.00	69
URCS-1242-25183	6.25	25.00	6.38	19.00	3.12	10.75	8.75	1.00	_	1.50	39.75	9.00	4" ANSI	2.00	87
URCS-1254-25184	6.25	37.00	6.38	25.00	3.12	10.75	11.75	1.00	_	1.50	51.75	9.00	4" ANSI	2.00	105
URCS-1754-25185	8.00	34.50	8.75	25.00	4.50	14.00	14.88	1.25	_	2.00	53.00	12.88	6" ANSI	2.50	187

#### STANDARD CONSTRUCTION MATERIALS & RATINGS

Constructi	on Material	Optional Material	Standard Unit Ratings
Shell	Steel	Steel	Operating Pressure Tubes
Tubes	Copper	90/10 Cu. Ni. / S. Steel	100 psig
Baffle	Brass	Brass	Operating Pressure Shell 100 psig
End Bonnet	Cast Iron	Brass / Stainless Steel	Operating Temperature
Gasket	Vito	400 °F	

#### **SURFACE AREA**

Model	Surface Area in Sq.ft.						
Number	1 / 4" O.D.	3 / 8" O.D.					
Number	Tubing	Tubing					
URCS-830-25180	15.0	_					
URCS-1230-25182	_	21.5					
URCS-1242-25183	_	30.2					
URCS-1254-25184	_	38.8					
URCS-1754-25185	_	72.4					

# UCN, URCN, UCF & URCF Series installation & maintenance

Receiving / Installation

a) Inspect unit for any shipping damage before uncrating. Indicate all damages to the trucking firms' delivery person, and mark it on the receiving bill before accepting the freight. Make sure that there is no visible damage to the outside surface of the heat exchanger. The published weight information located in this brochure is approximate. True shipment weights are determined at the time of shipping and may vary. Approximate weight information published herein is for engineering approximation purposes and should not be used for exact shipping weight. Since the warranty is based upon the unit date code located on the model identification tags, removal or manipulation of the identification tags will void the manufacturers warranty.

- b) When handling the shell & tube heat exchanger, special care should be taken to avoid dropping the unit since mishandling could cause the heat exchanger to crack and leak externally. Mishandling of the unit is not covered under the manufacturers warranty. All units are shipped with partial wood/corrugated cardboard containers for safe handling.
- c) Storage: American Industrial heat exchangers are protected against the elements during shipment. If the heat exchanger cannot be installed and put into operation immediately upon receipt, certain precautions are required to prevent deterioration during storage. The responsibility for integrity of the heat exchanger(s) is assumed by the user. American Industrial will not be responsible for damage, corrosion, or other deterioration of the heat exchanger during transit

Proper storage practices are important when considering the high costs of repair or replacement, and the possible delays for items which require long lead times for manufacture. The following listed practices are provided solely as a convenience to the user, who shall make their own decision on whether to use all or any of them.

- 1) Heat exchangers not to be placed in immediate service, require precautionary measures to prevent corrosion or contamination.
- Heat exchangers made of ferrous materials, may be pressuretested using compressed air at the factory. Residual oil coating on the inside surfaces of the heat exchanger(s) as a result of flushing does not discount the possibility of internal corrosion. Upon receipt, fill the heat exchanger(s) with the appropriate grade of oil or apply a corrosion preventing inhibitor for storage.
- Corrosion protection compounds for interior surfaces for long term storage or other applications are applied solely at the request of customers. Upon request, American Industrial can provide a customer approved corrosion preventative if available when included in the original purchase order specifications.
- Remove all dirt, water, ice, or snow and wipe dry before moving heat exchanger(s) into storage. Heat exchangers are generally shipped empty, open drain plugs to remove any accumulated condensation moisture, then reseal. Accumulation of moisture usually indicates corrosion has already started and remedial action should be taken.
- Store in a covered, environmentally stable area. The ideal storage environment for heat exchangers is in a dry, low-humidity atmosphere which is sealed to prevent the entry of blowing dust, rain, or snow. Maintain in atmospheric temperatures between 70°F and 105°F (Large temperature swings may cause condensation and moisture to form on steel components, threads, shell, etc...) Use thermometers and humidity indicators and maintain the atmosphere at 40% relative humidity, or lower.
- d) Standard Enamel Coating: American Industrial provides its standard products with a normal base coat of oil base air cure enamel paint. The enamel paint is applied as a temporary protective and esthetic coating prior to shipment. While the standard enamel coating is durable, American Industrial does not warranty it as a long-term finish coating. It is strongly suggested that a more durable final coating be applied after installation or prior to longterm storage in a corrosive environment to cover any accidental scratches, enhance esthetics, and further prevent corrosion. It is the responsibility of the customer to provide regular maintenance against chips, scratches, etc... and regular touch up maintenance must be provided for long-term benefits and corrosion prevention.
- e) Special Coatings: American Industrial offers as customer options, Air-Dry Epoxy, and Heresite (Air-Dry Phenolic) coatings

at additional cost. American Industrial offers special coatings upon request, however American Industrial does not warranty coatings to be a permanent solution for any equipment against corrosion. It is the responsibility of the customer to provide regular maintenance against chips, scratches, etc... and regular touch up maintenance must be provided for long-term benefits and corrosion prevention.

- f) American Industrial recommends that the equipment supplied should be installed by qualified personnel who have solid understanding of system design, pressure and temperature ratings, and piping assembly. Verify the service conditions of the system prior to applying any shell & tube heat exchanger. If the system pressure or temperature does not fall within the parameters on model rating tag located on the heat exchanger, contact our factory prior to installation or operation.
- g) Plan the installation to meet the requirements indicated on the piping installation diagram as illustrated above. It is recommended to put the hot fluid to be cooled through the shell side and the cold fluid through the tube side. The indicated port assembly sequence in the installation diagram maximizes the performance, and minimizes the possibility of thermal shock. In instances where the fluids are required to be reversed, hot fluid in the tubes and cold fluid in the shell the heat exchanger will work with reduced performance. Installation may be vertical or horizontal or a combination thereof. However, the installation must allow for complete draining of the heat exchanger regardless of Two Pass or four pass construction. Complete drainage is important to prevent the heat exchanger from freezing, over-heating of a fluid, or mineral deposit buildup.

For removable bundle heat exchangers, provide sufficient clearance at the stationary tube-sheet end to allow for the removal of the tube bundle from the shell. Bonnet can be removed to aid in cleaning the tubes without disassembling the tube bundle. For more information please contact American Industrial.

h) It is recommended to use flexible hose wherever possible to reduce vibration and allow slight movement. However, hoses are not required. Hydraulic carrying lines should be sized to handle the appropriate flow and to meet system pressure drop requirements

